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PERFORMANCE ANALYSIS OF VARIATION OF COP, REFRIGERATING EFFECT, POWER, COMPRESSOR WORK WITH EVAPORATING TEMPERATURE FOR CONDENSING TEMPERATURE OF 500C

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ABSTRACT

As for the harmful and disastrous effects of the chloro-flouro carbons and hydro-flouro carbons on the stratosphere, researchers around the world are looking for their substitute and alternatives in refrigeration system. To be in line with them, the present project deals with the comparative analysis of various eco-friendly hydro-carbon refrigerants. In the present work, properties of R12, R134a, R290, R600, R600a and blends of R290, R600 and R600a were calculated using RefProp Beta v 7.0 software. The COP for the aforementioned refrigerants were then calculated theoretically and compared with each other. Later, the COP of the best performing hydro-carbon blend was calculated via simulation software. The evaluation showed that the performance of R290, R600, R600a and the blend of R290/R600/R600a (65%/25%/10%) as compared to R12 was found to be 7.196%, 2.076%, 2.166% and 10.980% more, respectively. Similarly, the performance of R290, R600, R600a and the blend of R290/R600/R600a as compared to R134a was found to be 2.651%, 6.228%, 2.166% and 6.274% more, respectively. Moreover, the best feasible refrigerant from the alternative hydrocarbon refrigerants was found to be the blend of Propane (R290), Butane (R600) and Iso-butane (R600a) in the proportion of 65%, 25% and 10% by volume respectively.


INTRODUCTION OF REFPROP SOFTWARE

Reference fluid properties are an acronym of Refprop. The national institute of standards and technology developed the program to calculate the transport and thermodynamics properties of important fluids and their mixtures. These properties can be displayed in plots and tables through the graphical user interface. Refprop software is based on the most accurate mixture models and pure fluid. It implements thermodynamic properties of pure fluids three models are following:

1. Model of an extended corresponding states (ECS).
2. Helmholtz energy of the mixture components calculations employs the model that applies mixing rules.
3. Modified Benedict-Webb-Rubin equation of state. The equations of state explicit in Helmholtz energy. Viscosity and thermal conductivity are modeled with fluid specific correlations, the friction theory method or an ECS method. Helmholtz energy of the mixture components calculations employs a model that applies the mixing rules. It uses departure function to account for departure from ideal mixing. This software package were supported by reference the data program of NIST standard and the NIST thermos-physical properties division. The air conditioning and refrigeration technology institute the U.S. department of energy was supported to Refprop. The NIST have been supported over a period of many years by the numerous sponsors to the heating. U.S. department of energy, the electric power research institute, national laboratory, the environmental protection agency, refrigerating and air conditioning engineers, and the building environment and NIST divisions of thermos-physical properties.

CYCLE_D SIMULATION SOFTWARE

CYCLE_D simulates vapour compression refrigeration cycles that use single-compound refrigerants or refrigerant blends. The model can simulate a basic subcritical or transcritical refrigeration cycle, both with or without a liquid-line/suction-line heat exchanger. In addition, the model can simulate a subcritical two-stage economizer cycle, a subcritical three-stage economizer cycle, and a subcritical two-stage compression cycle with intercooling. CYCLE_D includes 62 single-compound refrigerants and 66 predefined blends. Single-compound fluids can be combined to form blends of up to five components. Computationally, the program is fully compatible with the NIST Reference Fluid Thermodynamic and Transport Properties Program - REFPROP, Version 9.0.
The basic subcritical or trans-critical system simulated by CYCLE_D consists of a compressor, a discharge line, a condenser for the subcritical cycle (a gas cooler for the trans-critical cycle), an expansion device, an evaporator, a compressor suction line, and an optional liquid-line/suction-line heat exchanger. The other subcritical cycles may contain a second compressor, and one or two economizers or an intercooler (but do not include the liquid-line/suction-line heat exchanger). The user of the program has to specify the refrigerant and provide input data for the above hardware components, except the expansion device, which is modeled as being isenthalpic. The user can also specify the power requirements of the indoor fan, outdoor fan, and control unit of the system.

A. Simple Vapour Compression Refrigeration System

shows the figure 2 systematic diagram of a simple vapour compression refrigeration system.
RESULTS AND DISCUSSION
In this chapter, result and discussion for the data obtained through NIST’s REFPROP 7.0 beta software, Cycle_D software and manual evaluation is carried out. Performance of Hydrocarbon Refrigerant.

![Graph 1](image1.png)

*Fig. 3 Variation of refrigerating effect with evaporating temperature for condensing temperature of 50°C*

![Graph 2](image2.png)

*Fig. 4 Variation of COP with evaporating temperature for condensing temperature of 50°C*
On theoretical evaluation, the performance of R290, R600, R600a and the blend of R290/R600/R600a (65%/25%/10%) as compared to R12 (Chloro-flouro Carbon) was found to be 7.196%, 2.076%, 2.166% and 10.980% more, respectively. Similarly, the performance of R290, R600, R600a and the blend of R290/R600/R600a as compared to R134a (Hydro-flouro carbon) was found to be 2.651%, 6.228%, 2.166% and 6.274% more, respectively.

However, the performance of the blend (R290/R600/R600a) as calculated through simulation using cycle_D software was found to be 2.54.

REFERENCES


